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# An overview of the mechanisms of $NO_x$ reduction with oxygenates over zeolite and $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalysts

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#### **Abstract**

The selective reduction of  $NO_x$  with added oxygenates over BaNa/Y and Ag/Y zeolites and  $Ag/\gamma$ -Al<sub>2</sub>O<sub>3</sub> takes place via complex reaction pathways with a number of common crucial intermediates. Acetate ions are formed by the oxidation of acetaldehyde over these catalysts. These acetate ions react with  $NO_2$  to form nitromethane which decomposes to HNCO via a dinitro- $C_1$  intermediate. HNCO hydrolyzes to form  $NH_3$  which can react with HONO to form ammonium nitrite. This  $NH_4NO_2$  efficiently decomposes to  $N_2$  and  $H_2O$  at  $100\,^{\circ}C$ , and at even lower temperatures in an acidic environment. The neutral surface species are expected to be in equilibrium with their ions. The rate-limiting step in these reaction sequences is the reaction of acetate ions to form nitromethane. When nitromethane is directly added to a  $NO_x$  stream over  $N_2$ 00% conversion of  $NO_x$ 100% to  $N_y$ 2 is achieved at temperatures as low as  $N_y$ 20. In such schemes,  $N_y$ 30 acts as a reductant of nitrate ions, ammonium nitrate and nitric acid. The benefits of isotopically labeled compounds in the elucidation of such reaction mechanisms and for providing insights into reaction dynamics are also discussed.

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### 1. Introduction

In industrialized countries, regulations limit emissions of toxic nitrogen oxides, carbon monoxide and unconverted hydrocarbons from automotive internal combustion engines. Worldwide, the introduction of catalytic converters, which detoxify the tail gas from gasoline-fired internal combustion engines, has markedly improved the quality of air in cities. Recent legislation in Europe and the U.S. places more stringent regulations on the emissions from vehicles powered by diesel engines. This remediation will require novel catalysts, since the traditional "three way catalyst" used for internal combustion (or "Otto") engines is unable to efficiently clean the tail gas from diesel engines. Diesel emissions contain several percent of O<sub>2</sub>, but almost no reducing gas; moreover, the temperature of diesel emissions is much lower ( $\sim 200$  °C) than that of the tail gas from Otto engines. The requirements for the catalytic abatement of nitrogen oxides from diesel emissions, therefore,

- (1) the catalyst has to be more active and
- (2) A reductant has to be provided.

Moreover, a catalyst for "cleaning" diesel tail gas also has to be *highly selective*, directing the added reducing agent(s) towards  $NO_x$  (present as a few hundred ppm) rather than  $O_2$  (present as several %). The catalyst must also be active in the presence of water vapor, and direct  $NO_x$  reduction to the desired products:  $N_2$  and  $H_2O$ . The reduction of  $NO_x$  is known to include a number of steps. With many catalysts of practical interest the final step is the formation of  $N_2$  by decomposition of ammonium nitrite [1-3]:

$$NH_4NO_2 \Rightarrow N_2 + 2H_2O \tag{1}$$

Decomposition of NH<sub>4</sub>NO<sub>2</sub> occurs efficiently at 100 °C, and at even lower temperature in an acidic environment [3]. Formation of ammonium nitrite takes place in the presence of ammonia

differ significantly from those for Otto engines in two important respects:

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which acts as a reductant. Three basic strategies have been described to provide this reductant:

- (a) Ammonia injection (e.g. by decomposing urea present in a urea/water slurry) into the tail gas.
- (b) Reduction of  $NO_x$  that has been trapped on an oxide surface as nitrates, to ammonia by intermittent exposure to a reducing gas.
- (c) Injection of a convenient reductant in combination with a selective catalyst that will reduce  $\sim 50\%$  of the NO<sub>x</sub> to NH<sub>3</sub>. This ammonia then acts as a reductant for the remaining NO<sub>x</sub>.

While the present paper focuses on issues and data directly related to strategy (c), it also provides data that are of relevance to strategies (a) and (b).

In previous publications we and others have shown why zeolite-based catalysts, such as BaNa/Y, are promising for  $NO_x$  reduction [1,4]. Though information on the molecular level details of the mechanisms for the selective catalytic reduction of  $NO_x$  is still sparse, the amount of information in this area in the literature is growing; both in terms of the systems considered and the extent of mechanistic detail [1–11].

For example, we have shown that  $NO_x$  reduction over BaNa/Y, can take place via two *parallel* routes, one involving free radicals, the other ionic adsorbates in equilibrium with the neutral parent molecules. With acetaldehyde as the primary reductant, the reaction intermediates include *nitromethane*, *dinitro-methane*, *formo-hydroxamic acid*, *isocyanic acid*, *ammonia*, *and ammonium nitrite* [1]. Previously published studies have focused on the reaction mechanism for individual systems. Specifically, we have studied the reaction mechanisms that are operative for  $NO_x$  reduction over  $Ag/\gamma$ - $Al_2O_3$ , BaNa/Y and Ag/Y zeolites [1,6,7].

The present paper takes a broader view of the operative mechanistic issues than prior publications on the aforementioned systems. The present work focuses on comparisons between the mechanisms and kinetics that are operative in these different systems. Such comparisons serve to highlight similarities and differences of the deNOx chemistry. A comparison of data from these systems allows identification of the rate-limiting step for deNOx chemistry. Once the ratelimiting step is identified an intermediate formed subsequent to this step, nitromethane, is an obvious choice as a reductant. The efficacy of nitromethane as a reductant has been validated by direct testing-nitromethane is an excellent low temperature NO<sub>x</sub> reductant, with an efficiency approaching 100% at temperatures as low as 140 °C. We also discuss results on the ability of NO to reduce a variety of relatively undesirable nitrates in NO<sub>x</sub> streams to more chemically reactive, and thus more desirable, nitrites.

# 2. Experimental

The apparatus and experimental approach have been described in detail in recent publications [1,7]. Briefly, catalyst samples were studied by transmission mode infrared spectroscopy using a homemade static cell. Some

experiments employed time resolved IR spectroscopy in a rapid scan mode. Since the zeolite and alumina samples are highly scattering powders, a very thin sample was used for transmission spectroscopy. However, it is extremely difficult to form a pellet of such material that is simultaneously self-supporting and thin enough for transmission IR studies. Our samples are prepared by "painting" a thin layer of sample from a slurry onto a heated tungsten wire grid clamped between two nickel jaws. The temperature controlled grid, which is highly transmissive, acts as a "scaffold" to support the very thin film of catalyst and allow for transmission IR studies. The catalytic activity of the samples was also probed with a temperature controlled micro flow reactor which is described in more detail in references [1.5.8].

#### 3. Basic catalytic chemistry

Many strategies for low temperature  $NO_x$  abatement have in common that  $NO_x$  is converted to ammonium nitrite; a compound that was shown by Millon, 160 years ago [12], to readily and efficiently decompose to  $N_2$  and  $H_2O$  at low temperature. In 1931, Abel et al. [13] showed that in the presence of a mineral acid, decomposition of ammonium nitrite even takes place at room temperature. As strong acids will liberate nitrite anions from ammonium nitrite, Abel et al. describe the observed kinetics at 25 °C by Eq. (2).

$$d(N_2)/dt = k[NH_4^+][NO_2^-][HNO_2]$$
 (2)

Since mineral acids will protonate ammonium nitrite, it is plausible that reaction (1) actually proceeds in two steps with protonated nitrosamine [H<sub>2</sub>NNOH]<sup>+</sup> being an intermediate. As Abel et al. studied aqueous solutions, we determined the temperature dependence of the decomposition of ammonium nitrite (reaction (1)) for solids by impregnating quartz powder or an active BaNa/Y catalyst with ammonium nitrite and recording the temperature-programmed decomposition of ammonium nitrite on either support [2]. Our data show that on these supports (in the absence of a strong acid), decomposition to  $N_2 + H_2O$  takes place near 100 °C. To examine the effect of solid acids, we studied physical mixtures that consisted of the acid zeolite, HY with ammonium nitrite covered BaNa/Y powder [3]. We found that after 13 h at 25  $^{\circ}$ C, >80% of the  $NH_4NO_2$  decomposed to  $N_2 + H_2O$ . This shows that surface diffusion of acid protons and/or ammonium nitrite suffices to enable the solid acid-catalyzed reaction (1) to occur at low temperature [3].

Thus, production and decomposition of ammonium nitrite add up to a potential route to  $N_2$  formation. One strategy for production of ammonium nitrite is the addition of ammonia to a  $NO_x$  stream. Our prior data demonstrate that one N atom in the  $N_2$  produced in such a scheme comes from  $NH_3$  and the other from  $NO_x$  [14]. *In situ* conversion of nitrogen oxides with ammonia is optimized when NO,  $NO_2$  and  $NH_3$  are present in a 1:1:2 ratio enabling the stoichiometric reaction [5]:

$$NO + NO_2 + 2NH_3 + H_2O = 2NH_4NO_2.$$
 (3)

Water is always present in diesel exhaust, but, in general, an exhaust gas flow interacting with a catalyst will not have the stoichiometry of reaction (3). Additional reactions therefore become important to convert the actual exhaust gas into the optimum mixture for reaction (3). For example, in practical applications some NO, which is normally in excess, may have to be converted to NO<sub>2</sub>.

As using aqueous urea to feed ammonia into exhaust streams (a proposed scheme for on-board  $NH_3$  production) has some drawbacks for motor vehicles, the present paper focuses on catalysts which are able to produce the ammonia required for reaction (3) in situ from  $NO_x$  and an appropriate reductant. In a diesel-fueled vehicle this reductant could be injected into the gas emitted by the engine. The desirability of an equimolar ratio of  $NO:NO_2$  and the role of NO in the overall reaction mechanism, which until recently was not widely appreciated [5], will be discussed in Section 4.

An important issue in  $NO_x$  SCR is the nature of the species formed on the catalyst upon exposure to a  $NO_x$  stream. Decomposition and/or reaction products can potentially block catalytically active sites. Our data [5] show that, in particular, nitrates are potential "catalyst poisons", but they can be efficiently reduced to nitrites by NO:

$$[N{O_3}^-]_{ads} + N{O_{gas}} \rightarrow [N{O_2}^-]_{ads} + N{O_{2,gas}} \tag{4}$$

For the catalysis under investigation, this is crucial, because chemisorbed  $NO_3^-$  ions, which can be produced from dissociative chemisorption of  $N_2O_4$  (reaction (5)), could block the surface sites required to catalyze reaction (1).

$$N_2O_4 \to NO_3^- + NO^+$$
 (5)

 $N_2O_4$  is formed via dimerization of  $NO_2$ . The formation of  $NO_3^-$  upon exposure of a BaNa/Y zeolite to  $NO_2$  is shown in Fig. 1. It also takes place on Ag/Y and Ag/ $\gamma$ -Al $_2O_3$  [6,7]. The counter ion in reaction (5),  $NO^+$ , has also been observed on BaNa/Y [1] and studied previously on related zeolites [15]. Subsequent to production by (4),  $NO_2^-$  can combine with  $NH_3$  and  $H^+$  that is present to yield  $NH_4NO_2$ . Thus, reaction (4) converts a potential "catalyst poison" into a desired reaction intermediate. Below we will present data of relevance to these and other reactions of NO.

# 4. NO as a reducing agent

Ammonia has been shown to be an efficient reductant for  $NO_x$ . In fact, in the systems we have studied, the added organic reductant provides a pathway for the *in situ* production of ammonia. As discussed below and elsewhere [5], both HONO and HNO<sub>3</sub> are expected to be present in realistic  $NO_x$  systems, which will contain water. Reaction of nitrous acid with  $NH_3$  leads to the formation of thermally labile ammonium nitrite, whereas reaction of  $NH_3$  with nitric acid leads to the formation of thermally more stable ammonium nitrate.

In prior work, we found that NO is an efficient reductant for nitric acid and surface nitrates [5]. Our studies of the reduction of  $NO_x$  with ammonia led to the reaction mechanism

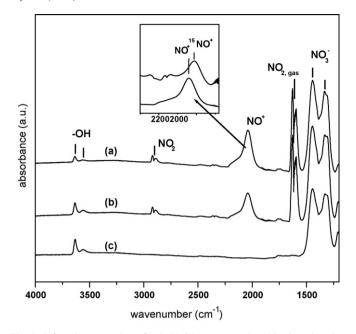
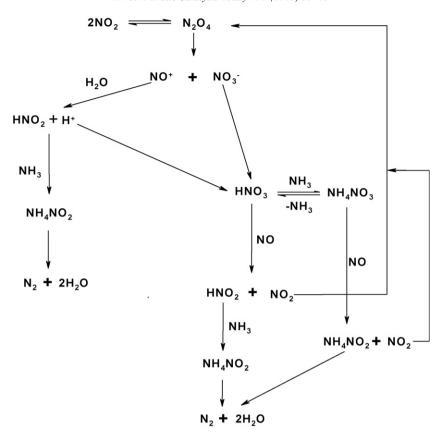


Fig. 1. Infrared spectra taken after BaNa/Y was exposed to  $NO_2$  (introduced as a mixture of  $NO + O_2$ ) at 200 °C. (a) after 1 min, (b) after 3 min, (c) after 9 min and subsequent to evacuation of IR cell. The insert is an expansion of the region in which the absorption due to  $NO^+$  is observed. The top trace is a spectrum taken exposure of Ba/Y was exposed to a mixture of  $^{15}NO + O_2$  at 200 °C.

summarized in Scheme 1 (reproduced with permission from Ref. [5]). This mechanism contains two major branches. In the branch on the left, NO<sup>+</sup>, produced in reaction (5), reacts with water to form HONO. Data showing that NO<sup>+</sup> and NO<sub>3</sub><sup>-</sup> ions form on a BaNa/Y zeolite surface simply by exposure of that surface to NO<sub>2</sub> are shown in Fig. 1. NO<sup>+</sup> is quite stable in the absence of water: at 200 °C the NO<sup>+</sup> absorption has been observed for up to 3 h [1]. However, NO<sup>+</sup> rapidly reacts with water to form HONO and H<sup>+</sup>, thus acting as a source for nitrous acid. This reaction also produces OH groups whose infrared absorption bands can be seen in Fig. 1. The HONO that is formed can then react with NH3 to give NH4NO2. The chemistry detailed in reaction (1) then prevails. The right hand branch of the scheme is more complex and deals principally with the fate of NO<sub>3</sub><sup>-</sup>, which can react with a proton to form nitric acid (HNO<sub>3</sub>), which can then react with ammonia to form ammonium nitrate.

As indicated in Scheme 1, our data demonstrate that NO reduces HNO<sub>3</sub> to HONO [5] which can then react with NH<sub>3</sub>, thus providing another reaction path to NH<sub>4</sub>NO<sub>2</sub>. Similarly, NO reduces surface nitrates to surface nitrites which are generally more thermally labile and thus less likely to act as a "poison" for the operative catalysts [5]. Finally, we have recently shown that NO can also efficiently reduce ammonium nitrate under acidic conditions [16]. The chemical nature of the catalyst surface affects the efficiency of and temperature at which this acid catalyzed reaction takes place. Unsupported solid NH<sub>4</sub>NO<sub>3</sub> is not appreciably reduced by contact with NO below its melting point of 170 °C, but when NH<sub>4</sub>NO<sub>3</sub> is supported on an even mildly acidic material, such as BaNa/Y, H–Y, or quartz, reduction of NH<sub>4</sub>NO<sub>3</sub> by NO is easily detectable at ~100 °C. Data showing a comparison of the



Scheme 1. This Scheme is reproduced by permission from: Journal of Catalysis 231, Y.H. Yeom, J. Henao, M.J. Li, W.M.H. Sachtler and E. Weitz "The role of NO in the mechanism of NO<sub>x</sub> reduction with ammonia over a BaNa-Y catalyst", 181–193, copyright 2005, Elsevier Inc.

temperature dependence of the reduction of ammonium nitrate on BaNa/Y versus neat ammonium nitrate is shown in Fig. 2. It is clear that the presence of BaNa/Y lowers the temperature at which reduction takes place. The mechanism involved in the reduction of NH<sub>4</sub>NO<sub>3</sub> by NO is treated in more detail in Ref. [16], which includes a discussion of the role of acid sites in the reduction of ammonium nitrate. However, the proposed mechanism can be summarized as follows: NH<sub>4</sub>NO<sub>3</sub> is in dissociative equilibrium with NH<sub>3</sub> and HNO<sub>3</sub> [9,17,18]. Brønsted and Lewis acid sites reversibly bind NH3 to form NH<sub>4</sub><sup>+</sup> (or NH<sub>3</sub>A<sup>+</sup>) [16]; thereby "freeing up" HNO<sub>3</sub> to be reduced by NO to HNO<sub>2</sub> [5,9] thus providing an indirect path, via the equilibrium indicated in Scheme 1, for NH<sub>4</sub>NO<sub>3</sub> to be reduced by NO at 100 °C in the presence of acids. Finally, the reversible binding of NH<sub>3</sub> to acid sites allows NH<sub>3</sub> to leave and recombine with HNO2 to form NH4NO2, which readily decomposes to  $N_2$  and  $H_2O$  at  $\sim 100$  °C [3]. Thus, we conclude that below its melting point the dominant mechanism for NH<sub>4</sub>NO<sub>3</sub> reduction by NO is via the equilibrium, shown in Scheme 1, between NH<sub>4</sub>NO<sub>3</sub> and HNO<sub>3</sub>. However, above the melting point, we cannot exclude direct reduction of NH<sub>4</sub>NO<sub>3</sub> by NO. This direct reduction channel is shown in Scheme 1.

As discussed in Ref. [5], the optimal NO:NO<sub>2</sub>:NH<sub>3</sub> ratio of 1:1:2 for the deNOx chemistry with ammonia is consistent with the role of NO as a reductant. Deviation from the 1:1, NO:NO<sub>2</sub> ratio results in less efficient NO<sub>x</sub> reduction. Thus, NO is an efficient and important reductant in deNOx chemistry. Its reductive ability acts to "channel" the reaction mechanism

depicted in Scheme 1 along branches that lead to more efficient production of  $N_2$  instead of potential catalyst "poisons".

# 5. In situ production of ammonia from $NO_x$ and the SCR mechanism

# 5.1. The SCR mechanism

Since, as indicated above, ammonia is an efficient and selective reductant for NO<sub>x</sub>, one strategy for NO<sub>x</sub> SCR is the *in*-

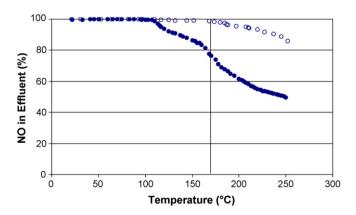


Fig. 2. Depletion of NO when NO is flowed over 0.2~g ground  $NH_4NO_3$  (open circles) and 0.2~g ground  $NH_4NO_3$  physically mixed with 0.15~g BaNa–Y (filled circles). The melting point of  $NH_4NO_3$  (170 °C) is designated by a vertical line. Flow rate is  $16.8~cm^3/min$  of a mixture of 2% NO in He.

situ production of ammonia by reduction with an appropriate organic molecule. Previously we had shown that over a BaNa/Y, Ag/Y and Ag/ $\gamma$ -Al $_2$ O $_3$  catalysts acetaldehyde is readily oxidized to acetate ions, which are subsequently converted to nitromethane [1,6,7]. These data imply that a di-substituted C $_1$  intermediate is formed in this reaction network. We have explained the acceleration of the rate of reaction of nitromethane in the presence of NO $_2$  [1,8] in terms of the sequence:

$$CH_3COO_{(ads)}^- \rightleftharpoons [CH_2 = CO_2_{(ads)}^-] + H$$
 (6)

This hydrogen atom abstraction could be facilitated by interaction of surface acetate with NO<sub>2</sub>, which would be followed by

$$[CH_2 = CO_{2(ads)}^{-}] + NO_2 \rightleftharpoons [O_2N - CH_2 - CO_2^{-}]$$
 (7)

and then by

$$[O_2N-CH_2-CO_2^{-}] \rightarrow CO_2 + [O_2N-CH_2^{-}]$$
 (8)

followed by

$$[O_2N-CH_2^-] + H^+ \to CH_3NO_2,$$
 (9)

where  $CH_2 = CO_2^-$ ,  $O_2N - CH_2^-$  and  $O_2N - CH_2 - CO_2^-$  are proposed intermediates.

Nitromethane can also be formed along a parallel route from acetaldehyde and NO<sub>2</sub>, initiated by formation of an acetyl radical:

$$CH_3CHO + {}^{\bullet}NO_2 \rightarrow HONO + {}^{\bullet}CH_3CO$$

$$^{\bullet}CH_3CO + ^{\bullet}NO_2 \rightarrow CO + CH_3NO_2$$

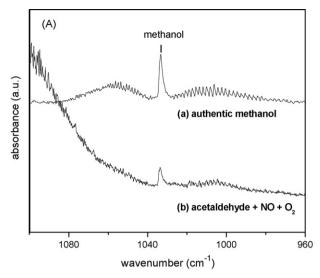
Evidence for a second parallel channel involving radical intermediates comes from a comparison of the chemistry that takes place with acetaldehyde and acetic acid as reductants [1].

Acetic acid forms surface acetate on contact with a variety of surfaces including BaNa/Y. The subsequent chemistry attributed to the ionic channel on BaNa/Y is identical with acetaldehyde and acetic acid as reductants. As expected, significant carbon dioxide formation is observed with acetic acid. Timing of the formation and isotopic labeling indicate that there are two primary steps for CO<sub>2</sub> formation: (1) the displacement of CO<sub>2</sub> by reaction of surface acetate with NO<sub>2</sub>, as shown in reaction (8), and (2) the formation of CO<sub>2</sub> on hydrolysis of HNCO, which is accompanied by ammonia formation via the reaction:

$$HNCO + H_2O \rightarrow NH_3 + CO_2$$
 (10)

As discussed below, and in reaction (11), HNCO is a product of the reaction of nitromethane and NO<sub>2</sub>.

With acetaldehyde as the reductant (but not with acetic acid) other products, including a significant amount of CO and methanol are observed. We have also shown that CO is not significantly oxidized to CO<sub>2</sub> over BaNa/Y under reaction conditions [1]. Fig. 3 presents data showing the formation of CO and methanol over BaNa/Y with acetaldehyde as a reductant. Formaldehyde is also a likely product. These products are attributed to the parallel radical reaction channel. A plausible mechanism that is consistent with formation of



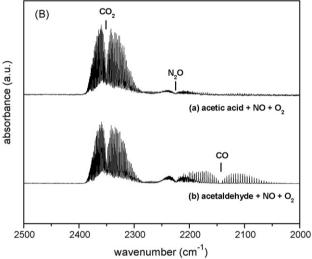


Fig. 3. Panel A: (a) The spectrum was taken after introduction of gas phase methanol into a IR cell. (b) Gas phase spectrum was obtained after BaNa/Y was exposed to a mixture of acetaldehyde + NO +  $O_2$  at 270 °C. Panel B: (a) A gas phase spectrum was recorded after BaNa/Y was exposed to acetic acid + NO +  $O_2$  at 200 °C. (b) A gas phase spectrum was recorded after BaNa/Y was exposed to acetaldehyde + NO +  $O_2$  at 200 °C.

methanol along with considerable CO formation is shown in Scheme 2. This mechanism also leads to the formation of nitromethane. Based on the observation of significant CO there is evidence for a parallel radical pathway with Ag/Y and Ag/ Al<sub>2</sub>O<sub>3</sub> as catalysts with acetaldehyde or ethanol as a reductant [6,7].

Nitromethane, once formed by either the ionic or radical pathways in any of the aforementioned systems, can then react with NO<sub>2</sub>:

$$CH_3NO_2 + NO_2 \rightarrow HNCO + H_2O + NO_2 \tag{11}$$

As evidenced by the results of experiments using <sup>15</sup>NO<sub>2</sub>, this reaction is not simply a NO<sub>2</sub> displacement reaction; rather NO<sub>2</sub> accelerates the reaction of nitromethane leading to formation of HNCO [1,8]. Though nitromethane can decompose on surfaces yielding HNCO under the conditions that have been studied, this reaction is slow relative to the reaction (11) with NO<sub>2</sub>

concentrations that are representative of meaningful deNOx conditions. Evidence has been presented that reaction (11) proceeds through a symmetric dinitromethane intermediate: (NO<sub>2</sub>)CH<sub>2</sub>(NO<sub>2</sub>), which is likely in equilibrium with its aci anion, with the equilibrium constant dependent on the nature of the catalyst, as the nature of the catalyst affects the ion-catalyst stabilization energy [1].

In the absence of NO<sub>2</sub>, nitromethane isomerizes to formohydroxamic acid, HCO–N(H)OH. Formo-hydroxamic acid loses water and becomes isocyanic acid:

$$CH_3NO_2 \rightarrow HCO-N(H)OH \rightarrow HNCO + H_2O$$
 (12)

HNCO can be readily hydrolyzed:

$$HNCO + H_2O \rightarrow NH_3 + CO_2 \tag{13}$$

The combination of reactions (11) and (13) or (12) and (13) thus produces the ammonia required for reaction (3). Under actual  $NO_x$  reduction conditions, the majority of  $NH_3$  must be formed via reactions (11) and (13) rather than reactions (12) and (13). Formation of ammonia allows for reaction with HONO to form ammonium nitrite, which as discussed above provides an efficient low temperature route to  $N_2$ .

Adding up reactions (12) and (13) shows that in the overall process nitromethane is efficiently converted to  $NH_3 + CO_2$ :

$$CH_3NO_2 \rightarrow NH_3 + CO_2 \tag{14}$$

Combining this with Eqs. (1) and (2) shows that over some catalysts  $NO_x$  is efficiently reduced by nitromethane:

$$2CH_3NO_2 + NO + NO_2 \rightarrow 2CO_2 + 2N_2 + 3H_2O$$
 (15)

As alluded to above, a pathway that is qualitatively very similar can be followed when ethanol is used as an added reductant over either  $Ag/\gamma$ - $Al_2O_3$  or Ag/Y zeolite [6,7]. As shown in reaction (16), ethanol can be converted to acetaldehyde by oxidation with  $O_2$ .

$$2C_2H_5OH + O_2 \rightarrow 2CH_3CHO + 2H_2O$$
 (16)

Once acetaldehyde is formed, the subsequent chemistry follows that seen when acetaldehyde is added as a reductant [7]. However, there is an important difference with ethanol. Ethanol can be oxidized by either  $O_2$  as shown above, or by  $NO_2$ . When oxidation by  $NO_2$  is dominant, as we have shown is the case for  $Ag/\gamma$ - $Al_2O_3$  at temperatures below 300 °C, ethyl nitrite is formed as an intermediate. Ethyl nitrite can dissociate to give acetaldehyde as a product, with the following reaction

mechanism proposed in the literature [19].

$$C_2H_5ONO \rightarrow C_2H_5O + NO$$
  
 $C_2H_5O + NO \rightarrow HNO + CH_3CHO$   
 $2HNO \rightarrow N_2O + H_2O$   
 $C_2H_5O + NOH \rightarrow C_2H_5OH + NO$ .

Ethyl nitrite can also dissociate to give  $N_2O$ —an undesirable greenhouse gas which sequesters  $N_2$ . Thus, as shown in Fig. 4, it is not surprising that ethyl nitrite is not as efficient a reductant for  $NO_x$  as acetaldehyde. Therefore, a key to efficient use of ethanol as a reductant is to identify a system in which ethanol is oxidized to acetaldehyde at low temperature. This can be accomplished with Ag/Y zeolite at  $\sim$ 320 °C. At this temperature ethanol leads to  $NO_x$  reduction approaching 80% [6].

In this paper, for simplicity, we have typically written reactions for neutral species unless we intend to emphasize the role of the ionic pathway. However despite differences between the catalytic systems we have studied, *in each of these cases nitromethane and/or its aci-anion is a crucial intermediate* [1,6,7].

Materials that are able to catalyze reaction (8) at a low temperature obviously hold important potential as deNOx catalysts. These considerations lead to a novel perspective and two resulting scenarios for  $NO_x$  abatement:

- Scenario 1: Nitromethane is produced in situ from NO<sub>2</sub> and an added reductant, such as acetaldehyde or ethanol.
- Scenario 2: Nitromethane is provided from an external source.

In previous papers we have shown that Scenario 1 described the chemistry of some promising catalyst systems. For example, acetaldehyde is easily oxidized to acetate ions by NO<sub>2</sub> over BaNa/Y catalysts:

$$CH_3CHO_{ads} + NO_2 \rightarrow [CH_3COO]_{ads}^- + H_{ads}^+ + NO$$
 (17)

The acetate ions react with the free radical  ${}^{\bullet}NO_2$ , forming the acetate radical ion,  $[{}^{\bullet}H_2C=CO_2]^-$ , which reacts with

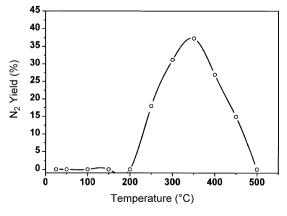


Fig. 4. The  $N_2$  yield as a function of temperature over 0.2 g Ag/ $\gamma$ -Al $_2$ O $_3$ . The mixture contained: 1100 ppm ethyl nitrite, 500 ppm NO $_2$ , 7% O $_2$ , 2% H $_2$ O at a GHSV of 18,000 h $^{-1}$ . The  $N_2$  yield is calculated based on the amount of NO $_2$  initially present.

another \*NO<sub>2</sub> molecule forming the ion [O<sub>2</sub>C-CH<sub>2</sub>-NO<sub>2</sub>]<sup>-</sup>. This intermediate rapidly loses CO<sub>2</sub>, becoming the aci ion of nitromethane. This chemistry can be summarized as follows:

$$[\text{CH}_3\text{COO}]_{ads}^- + 2\text{NO}_2 \rightarrow [\text{CH}_2\text{NOO}]_{ads}^- + \text{HONO} + \text{CO}_2$$

$$\tag{18}$$

This catalysis, producing nitromethane from acetate ions at the catalyst surface and impinging  $NO_2$  molecules, appears quite demanding. Therefore, we report below the results of experiments in which nitromethane was fed directly to the  $NO_x$  containing mixture.

If for a given catalyst the *in situ* formation of nitromethane from acetaldehyde is the rate-limiting step, it follows that the formation of  $N_2$  from nitromethane that is directly fed into a  $NO_x$  stream will be much faster and observable at a lower temperature. Flow reactor studies support this conclusion. Virtually 100%  $NO_x$  reduction can be achieved with nitromethane as an added reductant at temperatures as low as 150 °C over a Ag/Y zeolite catalyst [8]. Interestingly, the  $NO_x$  reduction yield is *not* significantly affected when the surface of the zeolite is pre-exposed to an acetate precursor, such as acetic acid, or when the surface sites are occupied by  $CN^-$  or  $NC^-$  [8]. In contrast, on BaNa/Y, a high coverage of surface acetate inhibits  $NO_x$  reduction [1].

Though still speculative and needing further study, these results suggest intriguing and important mechanistic conclusions regarding the microscopic details of the reaction of nitromethane with NO<sub>2</sub> relative to the reaction of NO<sub>2</sub> with surface acetate. The reaction of surface acetate with NO<sub>2</sub>

becomes less efficient as the coverage of acetate ions increases, implying that surface sites necessary for the reaction of NO<sub>2</sub> with acetate can be occupied by acetate [1]. This suggests a Langmuir-Hinshelwood mechanism for the reaction of acetate with NO<sub>2</sub>. However, surface acetate does not significantly affect the yield of N<sub>2</sub> when nitromethane is the added reductant [8]. This result suggests that the reaction of nitromethane with NO<sub>2</sub> takes place on a different set of sites than is used by strongly bound acetate ions in their reaction with NO<sub>2</sub>. Further, since acetate ions appear to block NO<sub>2</sub> adsorption, these results taken together suggest that the reaction of NO2 with nitromethane takes place via an Eley-Rideal mechanism. Hopefully, further studies will examine these conclusion which if confirmed will provide an even more detailed microscopic view of the overall reaction processes. These results also bring up the question as to whether nitromethane formed in the reaction of acetate with NO<sub>2</sub> migrates to other surface sites or whether there are multiple types of sites on which nitromethane can react. This is another issue for clarification in future studies.

# 5.2. Rate-limiting step(s)

Efficient  $NO_x$  reduction with acetaldehyde to  $N_2$  over BaNa/Y requires a temperature near 200 °C and even higher temperatures over Ag/Y and Ag/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> [6,7]. However, as discussed above and in Refs. [7,8],  $NO_x$  reduction to  $N_2$  proceeds with a high rate and a high nitrogen yield at 140 °C, when nitromethane is used as the primary reductant. Interestingly, the temperature at which  $NO_x$  reduction is initiated in the systems delineated above qualitatively correlates

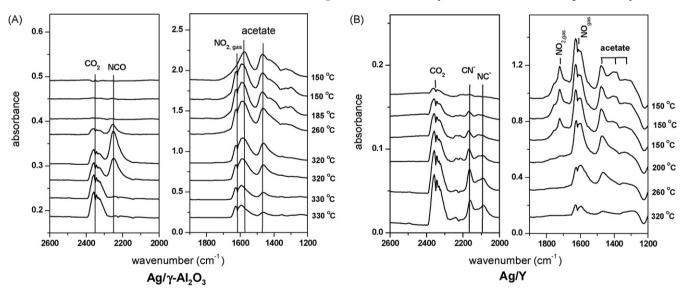


Fig. 5. The reactions of surface acetate on  $Ag/\gamma$ - $Al_2O_3$  and  $Ag/\gamma$  as a function of temperature. (Panel A)  $Ag/\gamma$ - $Al_2O_3$  was exposed to acetic acid and the gas phase acetic acid was then removed by evacuation. The top spectrum in was recorded after evacuation at 150 °C. After evacuation of the acetic acid, 4.9 Torr  $NO_2 + 60$  Torr  $O_2$  was introduced at 150 °C, and a spectrum was recorded at 150 °C. After recording the spectrum 150 °C the temperature was increased and spectra at the indicated temperatures were sequentially recorded. (Panel B)  $Ag/\gamma$  was pre-exposed to acetic acid and subsequently evacuated before the introduction of 5.9 Torr of  $NO_2$  (not shown here). From top to bottom, the elapsed time for the first three traces is: 1, 2, and 3.5 min (all at 150 °C). The temperature was then increased from 150 to 320 °C. The spectra, which were recorded sequentially are labeled by the temperature at which they were taken. This figure is reprinted from the Journal of Catalysis, (2006) 238 100 by Y.H. Yeom, M.J. Li, W.M.H. Sachtler and E. Weitz, entitled "A study of the mechanism for  $NO_x$  reduction with ethanol on  $\gamma$ -alumina supported silver", Figure 10, page 106, copyright 2006 with permission from Elsevier Limited and from the Journal of Catalysis (2007) 246 413 by Y.H. Yeom, M.J. Li, W.M.H. Sachtler and E. Weitz, entitled, "Low – temperature  $NO_x$  reduction with ethanol over Ag/Y: A comparison with Ag/g- $Al_2O_3$  and BaNa/Y", Figure 12 page 423, copyright 2007 with permission from Elsevier Limited.

with the temperature at which the reaction of surface acetate and  $NO_2$  becomes efficient. For example,  $NO_x$  is efficiently reduced to N<sub>2</sub> at 200 °C over BaNa/Y ( $\sim$ 90%) or Ag/Y ( $\sim$ 60%) while no  $NO_x$  is reduced over  $Ag/\gamma$ - $Al_2O_3$  at the same temperature. This is shown in Fig. 5 for Ag/Y and Ag/γ-Al<sub>2</sub>O<sub>3</sub> (not shown for BaNa/ Y). As can be seen in the Fig. 5, N-containing intermediates start to form at  $\sim 150$  °C over Ag–Y and at  $\sim 260$  °C over Ag/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. Reactivity of surface acetate and detailed assignments of absorption bands has been discussed in Refs. [6,7]. The combination of these results leads to the key point: There is efficient NO<sub>x</sub> reduction at temperatures that correlate with the reactivity of acetate with NO2, in a reaction that leads to nitromethane formation and there is very efficient (near 100%) for NO<sub>x</sub> reduction with nitromethane of Ag/Y at a temperature significantly below that where acetate reacts with NO<sub>2</sub>. In combination these results strongly suggests that formation of nitromethane is the rate-limiting step in NO<sub>x</sub> reduction over the catalysts in which nitromethane is produced via *in situ* reactions of added oxygenates [8].

# 5.3. Isotopic labeling

One of the paramount issues in applications of transient spectroscopy for the elucidation of reaction mechanisms is the identification of reaction intermediates. Often infrared is the spectroscopy of choice for such studies due to the chemical specificity of the IR absorption region (i.e. the fingerprint region). However, chemically similar species typically absorb in the same infrared region. In such cases, use of isotopically labeled compounds and the attendant shifts in the positions of infrared absorptions in these compounds can provide information that is critical to the successful identification of an intermediate. We have extensively employed isotopic labeling to allow us to identify intermediates in NO<sub>x</sub> SCR. For example, the isotopic shift on <sup>15</sup>N substitution in NO<sup>+</sup> (see Fig. 1) is in good agreement with literature values [1,20,21].

Isotopic labeling can also play an important role in the determination of reaction dynamics and reaction mechanisms. As an illustration, we have employed isotopically labeled acetic acid to probe the mechanism of  $NO_x$  SCR over BaNa/Y zeolite [1]. As alluded to above, the published mechanism for this process indicates that  $CO_2$  should be generated in two steps [1]: one is the replacement by  $NO_2$  of the carboxylic acid group bound to a Ba leading to the aci-anion of nitromethane (Eq. (19)),

$$CH_2COO^- + NO_2 \rightarrow CH_2NO_2^- + CO_2$$
 (19)

The other step leading to (the second) CO<sub>2</sub> is the hydrolysis of either HNCO, NCO or NCO<sup>-</sup> (Eq. (13) shows this for HNCO) which in turn is produced via the decomposition of dinitromethane and/or its aci anion. Eq. (20) below is shown for the neutral pathway for production of NCO.

$$CH_2(NO_2)_2 \rightarrow H_2O + NO_2 + NCO$$
 (20)

As alluded to in Section 5.1, the fact that there are two  $CO_2$  producing steps is confirmed by isotopic labeling [1]. Upon labeling one of the carbons in acetic acid, we observe that one  $CO_2$  being formed contains the label of the carboxylic acid

carbon and the other contains the label of the methyl carbon. Labeling of the  $NO_2$ , which is allowed to react with unlabeled nitromethane, provides additional mechanistic information. The observation that the resulting HNCO (see Eq. (11)) found in the presence of a 1:1 mixture of  $^{15}NO_2$  and  $^{14}NO_2$  is  $\sim$ 1:1  $\rm H^{14}NCO$  and  $\rm H^{15}NCO$ , strongly suggests a symmetric intermediate such as dinitromethane [1]. Finally, prior experiments using  $^{15}N$  demonstrated that one N in the  $N_2$  resulting from NH<sub>3</sub> SCR of  $NO_x$  came from the  $NO_x$  and one came from NH<sub>3</sub> [14]. These results implicate an intermediate that contains two N atoms and readily dissociates to  $N_2$ : as discussed in Section 3, ammonium nitrite fits these criteria.

# 6. Conclusions

A comparison of the mechanisms for the selective catalytic reduction of NO<sub>x</sub> with acetaldehyde or ethanol over different catalysts (BaNa/Y, Ag/Y and Ag-\gammaAl2O3) allows for the elucidation of similarities and differences in the mechanisms. The mechanisms for NO<sub>x</sub> reduction in these systems proceed by a route that is qualitatively similar and involves the formation of surface acetate ions which react with NO2 to form nitromethane. This crucial intermediate then reacts with NO2 to form dinitromethane, which rapidly decomposes to give HNCO. It is well known that HNCO readily hydrolyzes to give NH<sub>3</sub>, which can react with another HONO molecule to form ammonium nitrite. This ammonium nitrite then decomposes at low temperature (≤100 °C) to cleanly give N<sub>2</sub> and H<sub>2</sub>O. Further, NO is an efficient reductant for converting nitric acid, surface nitrates and ammonium nitrate to the respective nitrite. In each case, the result of the reduction reaction is to produce a mechanistically more desirable species that favors the production of thermally labile ammonium nitrite or surface nitrites as opposed to more thermally stable ammonium nitrate or surface nitrates. There is also strong evidence for a parallel pathway for formation of nitromethane in some systems that is initiated by the formation of acetyl radicals. Evidence for this pathway comes from a comparison of the chemistry that takes place with acetic acid versus acetaldehyde as the reductant. With acetic acid there is only evidence for formation of surface acetate and reactions of NO2 with acetate and subsequent intermediates. However, acetyl radicals that can form as a result of H atom abstracted by NO2 from acetaldehyde can readily decompose to methyl radicals with CO as a co-product. They can also react to yield products that are not observed with acetic acid as the reductant. The observation of a much higher CO/ CO<sub>2</sub> ratio and additional reaction products serves as a signature of this radical pathway.

One major difference among the systems that we have studied is the temperature at which deNOx chemistry takes place. This temperature can be correlated with the temperature at which acetate reacts with  $NO_2$  to form nitromethane, thus identifying this reaction as the rate-limiting step in the reaction mechanism. It follows that direct addition of nitromethane should lead to lower temperature SCR of  $NO_x$ . Indeed,  $N_2$  yields of  $\sim 100\%$  have been obtained at temperatures as low as  $140\,^{\circ}$ C. Further, the reaction of nitromethane is relatively

insensitive to the presence of surface acetate or CN<sup>-</sup> and NC<sup>-</sup>. These observations allow for some interesting speculations on the molecular level mechanistic details of the reactions of acetate and nitromethane with NO<sub>2</sub>.

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